

PROCESSING OF SHIPBOARD WASTEWATER

The present invention relates generally to processing of wastewater onboard a marine vessel, involving flashing of the wastewater into water vapor.

BACKGROUND OF THE INVENTION

Presently, liquid waste in the form of bilgewater is cleansed by processing systems which utilize ultrafiltration membranes to separate oil and water, as disclosed for example in U.S. Patent No. 5,932,091 to Tompkins et al. Such processing systems rely on fine-sized membrane pores which create high fouling rate problems so as to require use of flushing modes and heavy duty recirculating pumps to wash membrane surfaces in order to prolong membrane life. It is accordingly, an important object of the present invention to provide a processing system for cleansing wastewater such as oily bilgewater that avoids reliance on ultrafiltration membranes subject to fouling and an unduly shortened life in the absence of extensive back flushing operational modes.

SUMMARY OF THE INVENTION

In accordance with the present invention, wastewater is processed in a flash chamber under vacuum established within an upper section thereof by a vacuum pump. Before delivery to the flash chamber, the wastewater is preheated in a heat exchanger to enhance subsequent flashing thereof effected by entry through an orifice. Water vapor produced by such flashing rises into and fills the upper chamber section, while liquid waste oil droplets are deposited into a bottom section of the flash chamber. A de-mister filters out contaminants from the rising water vapor entering the upper section of the flash chamber and liquefied water vapor is collected therebelow during removal of such rising water vapor from the flash chamber in a superheated or

1 saturated condition for condensation by cooling. The water condensate and the waste oil are
2 respectively withdrawn by distillate and drain pumps under automatic level sensing switch
3 controls. The water condensate withdrawn by the distillate pump is conducted through an oil
4 content monitor for overboard discharge from a distillate tank, while the waste oil or
5 contaminants from the bottom of the flash chamber is delivered by the drain pump to a waste
6 storage tank to which the water condensate is delivered when an excessive amount of
7 contaminant is detected therein. Level sensors associated with the automatic pump drive controls
8 shut down the distillate pump when the water condensate within the distillate tank drops below a
9 predetermined level. On the other hand, the drain pump is turned on and off automatically under
10 level sensor control in order to prevent it from running dry and to maintain the vacuum inside the
11 flash chamber. An alarm is activated by a pressure sensor to alert the operator when the vacuum
12 in the flash chamber is lost. When the desired vacuum pressure is attained for flashing to occur,
13 the vacuum pump is automatically turned off under pressure control by the flash chamber
14 pressure sensor.

15
16 Pursuant to one embodiment of the invention, processing involves use of a condenser to
17 cool and condense the superheated and compressed water vapor withdrawn from the flash
18 chamber. Heat is transferred to the incoming wastewater during its initial passage in a heat
19 absorber coil through the rising water vapor within the lower section of the flash chamber. The
20 wastewater is then conducted from the condenser to the heat exchanger to undergo preheating
21 before delivery to the entry orifice in the flash chamber.

BRIEF DESCRIPTION OF DRAWING

A more complete appreciation of the invention and many of its attendant advantages will be readily appreciated as the same becomes better understood by reference to the following detailed description when considered in connection with the accompanying drawing wherein:

A schematic diagram depicts a wastewater processing system in accordance with one embodiment of the present invention, showing various components of the system interconnected by operational circuitry.

DETAILED DESCRIPTION OF PREFERRED EMBODIMENTS

Referring now to the drawing in detail, it diagrams a shipboard system for processing wastewater such as bilgewater or graywater received from a source such as a wastewater holding tank 10. According to the embodiment illustrated, the wastewater from the holding tank 10 is initially received through an inlet 14 into an inflow pump 12 for pressurization within a processor, generally referred to by reference numeral 16, from which an oil-free or contaminant free water condensate is obtained for overboard discharge through an outlet 18.

The wastewater from holding tank 10 after pressurization by pump 12 passes through a heat absorbing coil 20 located within a bottom section 21 of a flash chamber 22 in the processor 16. Heat from water vapor in the bottom section 21 is absorbed by the wastewater within the coil 20 before it is supplied to a condenser 26. The water vapor rising from the bottom section 21 when reaching an upper chamber section 23 of the flash chamber 22 after passing through a demister filter screen 46 is superheated and then withdrawn and compressed by a vacuum pump 28 for delivery in a superheated and compressed condition to the condenser 26 for cooling and condensation therein.

1 As the water vapor in the upper section 23 of the flash chamber 22 rises toward the
2 suction side of the vacuum pump 28, some of such water vapor will be liquefied when sensible
3 heat thereof is released. To collect such liquefied water vapor from the upper chamber section
4 23, a V-shaped trough 78 is formed within the flash chamber 22 below the upper section 23 into
5 which the liquefied water vapor drops through a slot 47 in alignment with the filter screen 46.
6 Two level sensors 77 detect upper and lower levels of liquefied water vapor collected in the
7 trough 78 by means of signals sent to a programmable logic controller 54 so as to turn on and off
8 a pump 79 through which the liquefied water vapor is withdrawn from the trough 78 and
9 delivered to vented distillate tank 38. The lowermost of the sensors 77 is located at a suitable
10 predetermined height above the bottom of the trough 78 to establish a lower liquid level
11 corresponding to a predetermined volume collected therein necessary to maintain a vacuum
12 pressure within the flash chamber 22 under operation of the vacuum pump 28. The latent heat of
13 condensation of the compressed and superheated water vapor delivered by the vacuum pump 28
14 from the upper chamber section 23 to the condenser 26 is accordingly transferred to the
15 wastewater within tubing in the condenser 26 from which the wastewater is then delivered for
16 further preheating to a heat exchanger 34. The condensate of the water vapor cooled in the
17 condenser 26 is also fed to the vented distillate tank 38 within the processor 16.

21 Rise of the water vapor within the upper section 23 of the flash chamber 22 is enhanced
22 by the vacuum maintained therein under operation of the vacuum pump 28, with the liquid waste
23 oil or contaminants deposited into and retained within a bottom section 21 of the flash chamber
24 22. Such waste oil or contaminants in the bottom section 21 is derived from the wastewater
25 heated in the condenser 26 and preheated further within the heat exchanger 34 to a predetermined
26 temperature level, such as approximately 175°, before delivery to the flash chamber 22 through
27
28

1 an entry orifice 44 to enhance flashing thereof within the flash chamber 22. A portion of such
2 wastewater which flashes into water vapor within the flash chamber 22 rises into the upper
3 chamber section 23. Heat is supplied for wastewater preheating to the heat exchanger 34 from a
4 suitable source 35, such as an existing hot water supply system or an electric heater, under control
5 of a temperature transducer 61 as hereinafter explained.

7 When sufficient heat is removed from the superheated and compressed water vapor within
8 the condenser 26 during performance of its cooling function as aforementioned, such water vapor
9 is condensed and delivered as a condensate to the distillate tank 38. Such condensate collected
10 within the distillate tank 38 is directly delivered from the condenser 26 after cooling and
11 condensation of the rising water vapor in the upper section 23 of the flash chamber 22 delivered
12 thereto by the vacuum pump 28. Oil mist or other liquid contaminants are filtered out by the
13 filter screen 46 (which is of a type generally known in the art) from the rising water vapor
14 entering the upper section 23 of the flash chamber 22 to limit the collection within the distillate
15 tank 38 to condensate free of such contaminate.

17 Oil and other contaminants in the bottom section 21 of the flash chamber 22, are
18 withdrawn therefrom by a drain pump 50 for storage in a vented waste storage tank 52 connected
19 by an outlet 76 to a relief valve 70 and a valve 68 through which the outlet of the drain pump 50
20 is delivered to the oil tank 52. Operational drive of the drain pump 50 is automatically regulated
21 through the programmable logic controller 54 aforementioned, in response to level sensors 67 on
22 the bottom section 21 of the flash chamber 22, set to maintain the desired vacuum pressure
23 therein as well as to prevent overflow of the flash chamber 22. Should the pressure in the flash
24 chamber 22 rise above a predetermine value, system shut-down is effected by the control 54, as
25 well as to sound an operator alerting alarm 56.

1 A distillate pump 58 is also provided for removal of condensate collected within the
2 distillate tank 38 from the condenser 26 and the liquid collection trough 78. The pump 58 directs
3 such condensate to the overboard discharge outlet 18 through an oil content monitor 60.

4 Automatic operation of the pump 58 is effected under control of the programmable logic
5 controller 54. Accordingly, when the condensate in the distillate tank 38 drops below a certain
6 predetermined level, as detected by a sensor 66, the pump 58 is turned off. When the condensate
7 then rises above another predetermined level in the distillate tank 38, the pump 58 is turned on to
8 prevent overflowing. Air venting devices 72 and 73 are respectively connected to the distillate
9 tank 38 and the condenser 26 to vent out non-condensate gases.
10

11 In regard to the upper section 23 of the flash chamber 22 in the processor 16, the rising
12 water vapor which is maintained under vacuum therein established by the vacuum pump 28, is
13 withdrawn by the pump 28 in a compressed condition to increase both its temperature and
14 pressure.
15

16 In regard to the control system associated with the processor 16, the temperature
17 transducer 61 associated with the controller 54 is set to maintain the wastewater operating
18 temperature at about 175 degrees Fahrenheit by controlling the source of heat 35 for the heat
19 exchanger 34. If the temperature goes up higher than the set operating temperature, the heat
20 source 35 will be turned off. If the temperature drops to 165 degrees Fahrenheit, heat source 35
21 will turn back on. The flash chamber level sensors 67 will have either a high or low setting.
22 When the level of oil in the bottom section 21 of the flash chamber 22 drops below a
23 predetermined level, a signal is sent to the programmable logic controller 54 which will turn off
24 the drain pump 50. If the level goes up to a predetermined level, it will turn on the drain pump
25 50. The level sensors 66 on the distillate tank 38 operate in the same way and also send an
26
27
28

1 electrical signal to the programmable logic controller 54 to turn on the pump 58. The level
2 sensors 66 on the distillate tank 38 thus operate to send an electrical signal to the programmable
3 logic controller 54 which in turn controls operation of the distillate pump 58. A pressure
4 transducer 65 controls operation of the vacuum pump 28 so that when the pressure drops to a
5 predetermined level, the vacuum pump 28 shuts off. Should the pressure rise above a
6 predetermined level at the suction side of the vacuum pump 28, the pressure transducer 65 sends a
7 signal to the programmable logic controller 54 to turn on the vacuum pump 28. In order to avoid
8 on and off cycling of the vacuum pump 28 during normal operation, the vacuum pump 28 will
9 also have a built in capacity controller. When the load varies, the vacuum pump 28 will
10 accordingly operate proportionately by automatically adjusting its own capacity to match the
11 load. When the pressure as detected by the pressure transducer 65 rises above a predetermined
12 level, a signal is sent to the programmable logic controller 54 to close valve 62 and open valve
13 63. In this way, all oil and other high viscous fluid emulsions are sent directly to the waste
14 storage tank 52, thus bypassing the flash chamber 22. Should the pressure rise above a
15 predetermined value set by the pressure transducer 75 for a predetermined time duration, a signal
16 is sent to the programmable logic controller 54 causing the processor 16 to go into a shutdown
17 mode.

18
19
20
21 Under the shutdown mode, the controller 54 will turn off the inflow pump 12. After such
22 turn off in a typical shutdown mode, the controller 54 will respond to existing conditions detected
23 by level sensors 67 and 66. Should the level sensors 67 and 66 indicate that levels are above their
24 respective low settings, the controller will turn on both the distillate and drain the pumps 58 and
25 50 until the fluid levels reach their predetermined low settings. Additionally, the controller 54
26
27
28

1 will also turn off the heat source 35 and the vacuum pump 28. The shutdown mode will therefore
2 occur only when the inflow pump 12 is not drawing suction from the wastewater holding tank 10.

3 Obviously, other modifications and variations of the present invention may be possible in
4 light of the foregoing teachings. It is therefore to be understood that within the scope of the
5 appended claims the invention may be practiced otherwise than as specifically described.
6

7 What is claimed is:
8
9
10
11
12
13
14
15
16
17
18
19
20
21
22
23
24
25
26
27
28